

A liquid-phase circulation-mode argon purification system

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High-purity noble liquids are difficult to procure, creating the need for on-site purification

Impurities in noble liquid detectors strongly deteriorate performance

→ Experiments perform purification themselves

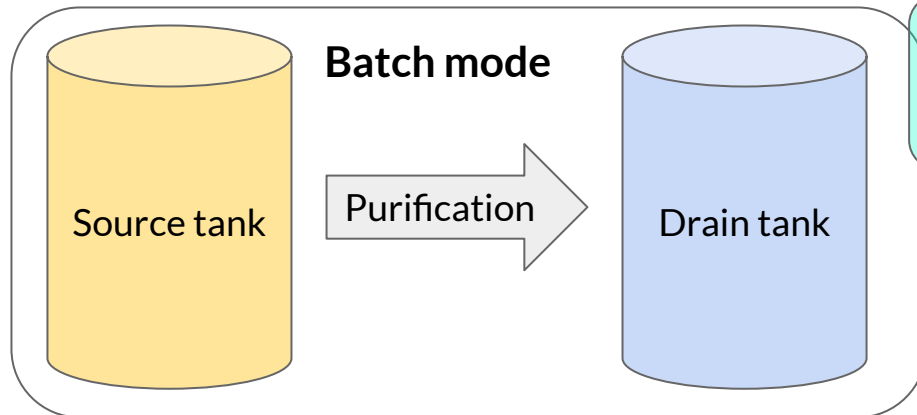
Noble liquids often not available in required purity (or expensive, in limited amounts, etc.)

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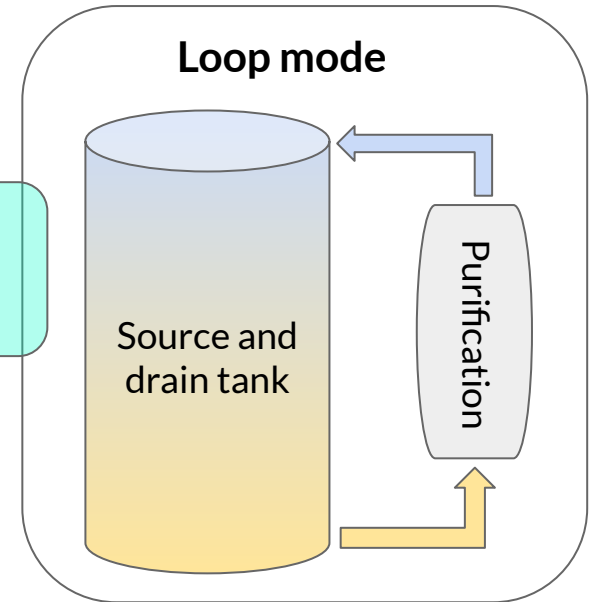
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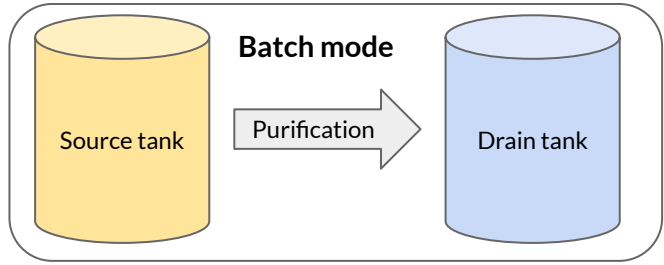
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Two purification modes possible!



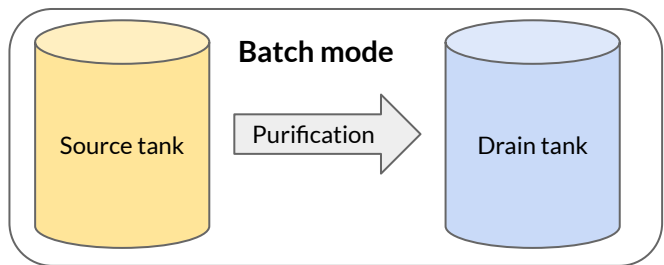
There are several modes in which noble liquids can be purified



Source tank \neq drain tank

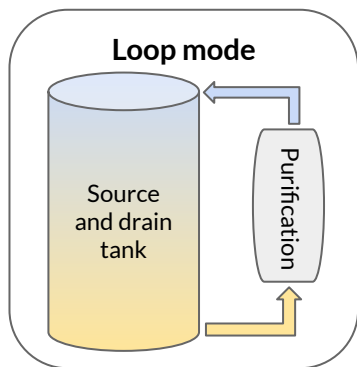
- ✓ Efficient
- ✓ Does not need a pump
- ✗ Needs two separate tanks
- ✗ only possible during detector filling, not possible during experimental runs

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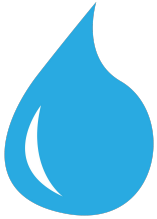
- ✓ Efficient
- ✓ Does not need a pump
- ✗ Needs two separate tanks
- ✗ only possible during detector filling, not possible during experimental runs



Source tank = drain tank

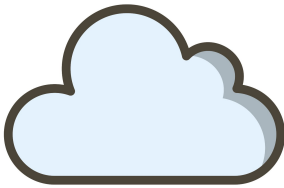
- ✗ Less efficient b/c impurities dilute
- ✗ Needs a pump
- ✓ Only needs one tank
- ✓ possible during experimental runs

In which phase to purify?



Liquid phase

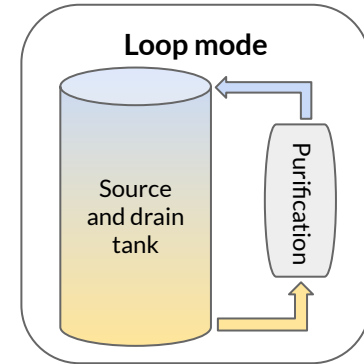
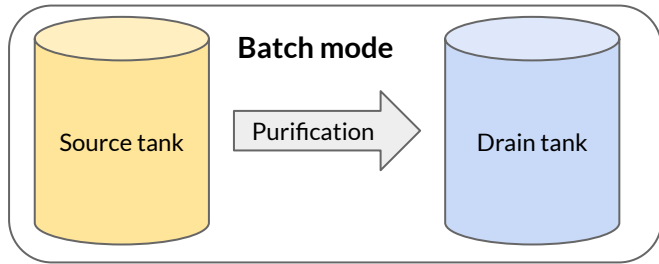
- ✓ No need to change phase (no boiling or condensing)
- ✓ High throughput due to high density
- ✓ Possible during detector filling in batch mode
- ✗ Less effective



Gaseous phase

- ✓ Very effective due to high mobility
- ✗ Need to change phase at least once (recondensing and/or boiling)
- ✗ Less throughput

Here: Purification in liquid phase and either batch or loop mode

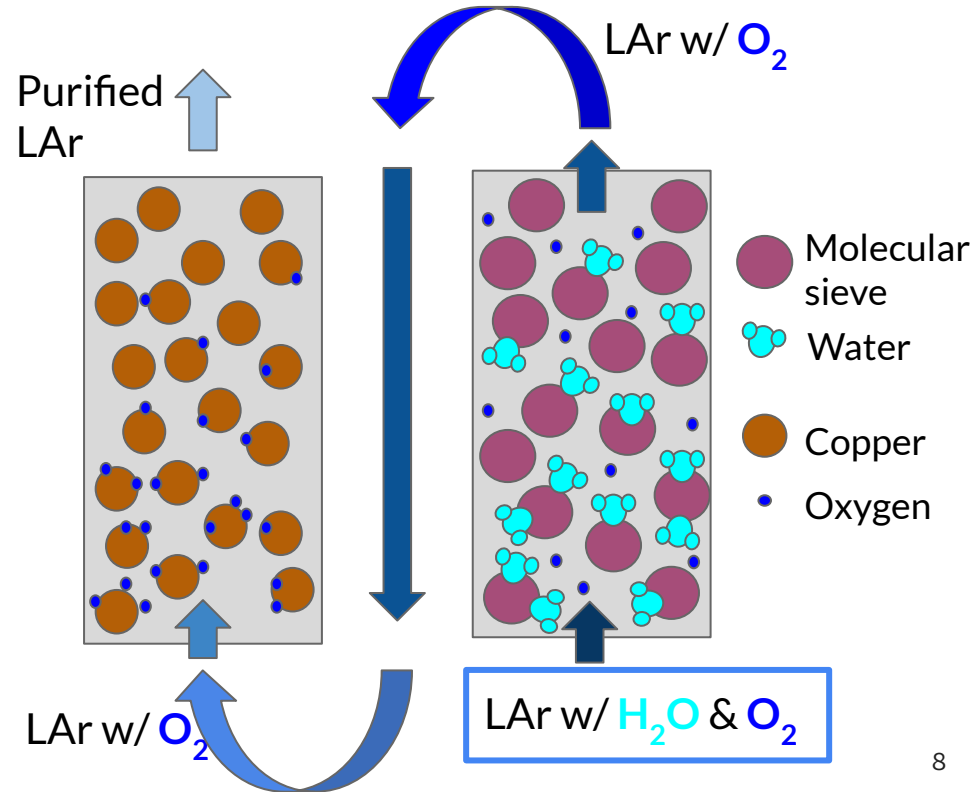


LAr can be purified with commercially available dispersed copper and molecular sieves

Water removal: Adsorption on molecular sieve with pore size of 4 Angstrom

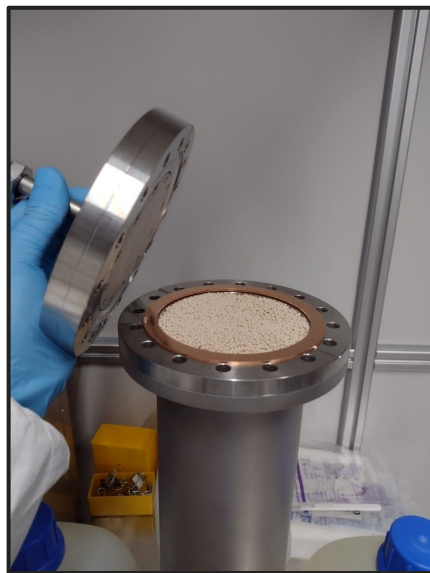
Oxygen removal: Chemical binding to copper via
 $2\text{Cu} + \text{O}_2 \rightarrow 2\text{CuO}$

Some nitrogen is retained as well



Filling of purification cartridges with molecular sieve and dispersed copper

Filled 2005 g of molecular sieve 4 A, and 2341 g of copper catalyst into stainless steel CF100 cylinders



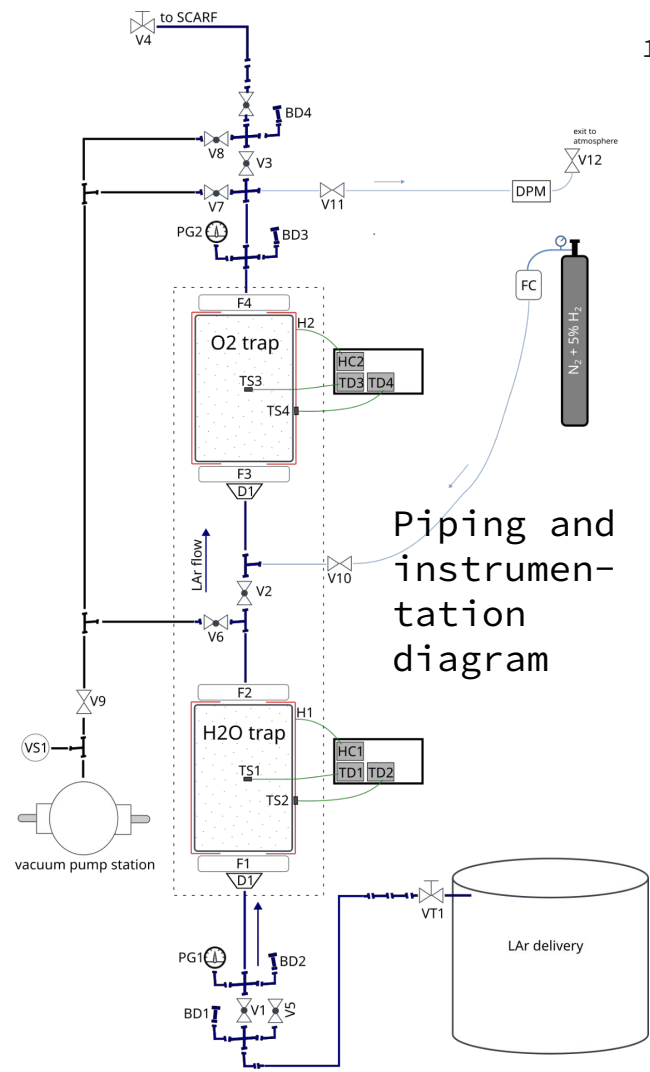
Piping and instrumentation



Purification setup w/o thermal insulation



CAD drawing of the purifier



Determination of the scintillation parameters with “LLAMA” – a triggered SiPM array

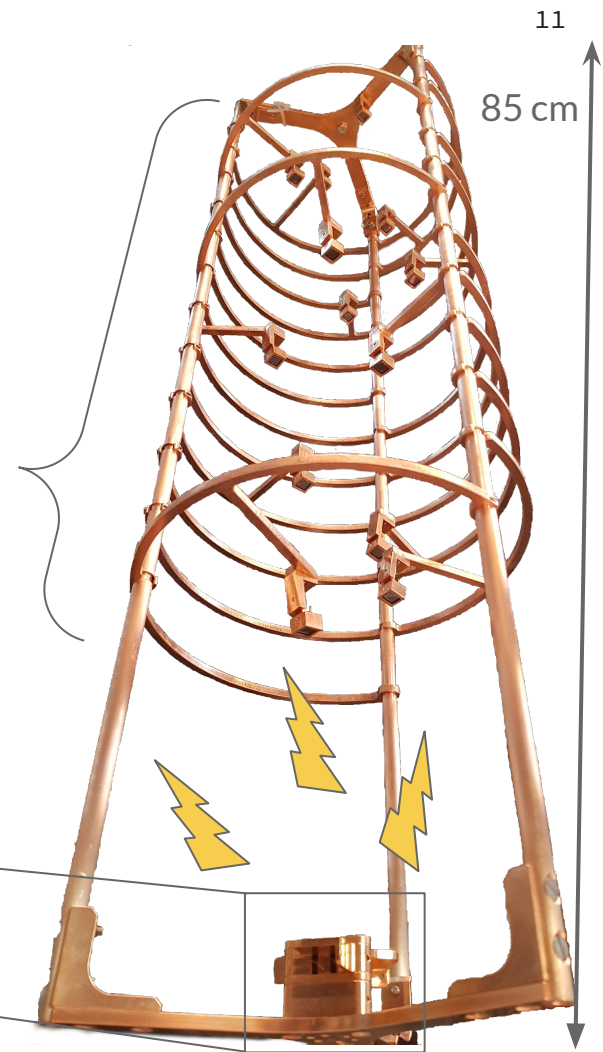
The LEGEND Liquid Argon Monitoring Apparatus (LLAMA) operates **completely submerged in LAr**, and features⁽³⁾

- ^{241}Am scintillation light source
- 3 “source” SiPMs providing the **trigger** and **p.e. yield**
- 13 peripheral SiPMs providing **time structure** and **propagation information**

³[M. Schwarz et al., *ANIMMA 2021* (July 2021)]

13 peripheral SiPMs pointing at the source

Scintillation source and 3 “source” SiPMs



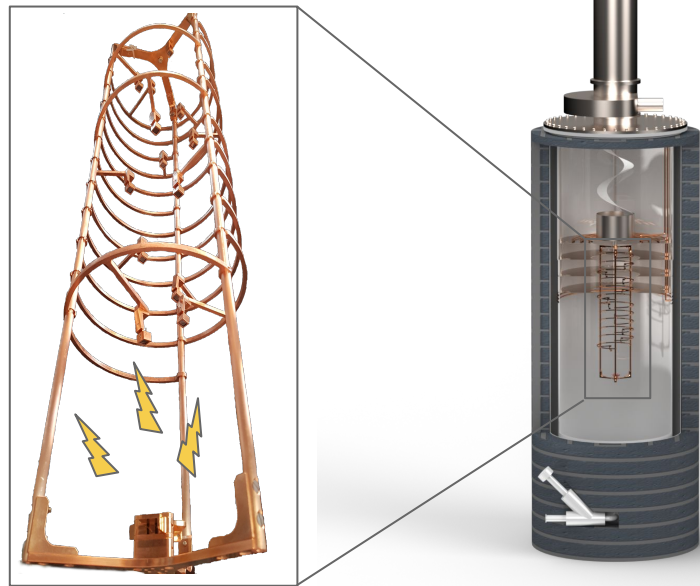
LLAMA is operating in SCARF, a 1 ton LAr test stand

Located in shallow underground laboratory
(depth of 10 m w.e.)

Muon flux reduced by factor of 4

Able to house LLAMA for various LAr
scintillation studies, e.g. XeDLAr at
LIDINE 2021: [C. Vogl et al 2022 JINST 17 C01031](#)

Alternative setup: Up to two germanium
detectors + fibers w/ SiPMs



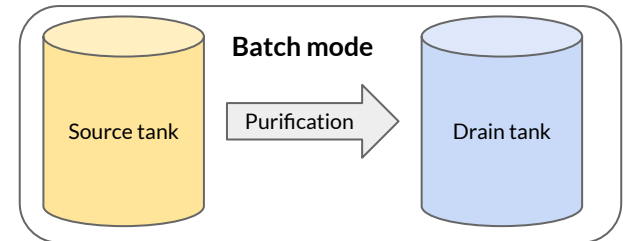
Application #1: Filling of “SCARF” cryostat



First performance test when filling 1 ton of LAr into empty cryostat “SCARF”

Initial impurities in delivered 600 L LAr tanks (vendor certificates):

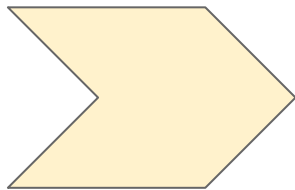
- 1) $[O_2] = 0.5 \mu\text{L/L}$
 $[N_2] = 0.5 \mu\text{L/L}$
 $[H_2O] < 3 \mu\text{L/L}$
- 2) $[O_2] = 0.2 \mu\text{L/L}$
 $[N_2] = 0.3 \mu\text{L/L}$
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Application #1: Filling of “SCARF” cryostat

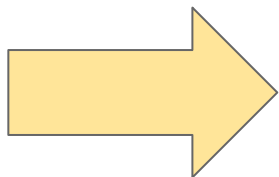
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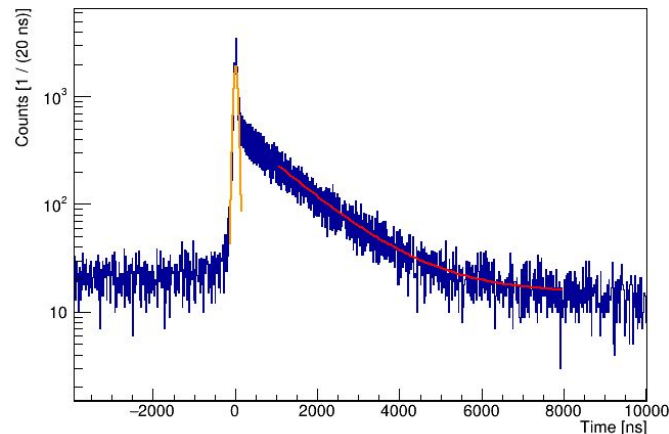
Measured triplet lifetime after purification:
 $1.31 \pm 0.02 \mu\text{s}$

Corresponds to^(1, 2)
< $0.01 \mu\text{L/L O}_2\text{-equiv.}$
and < $0.8 \mu\text{L/L N}_2$



**Successful purification
of 1 ton of LAr!**

Relative time position for energy>cut for SiPM 5



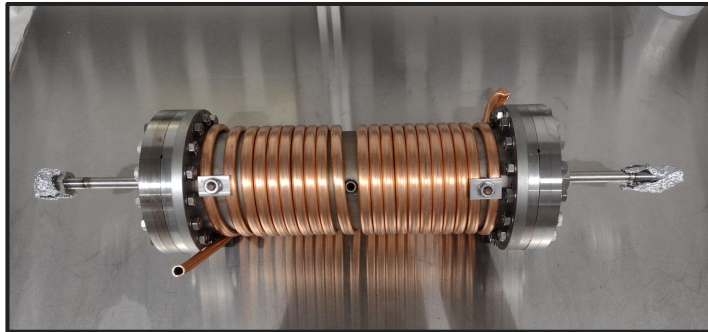
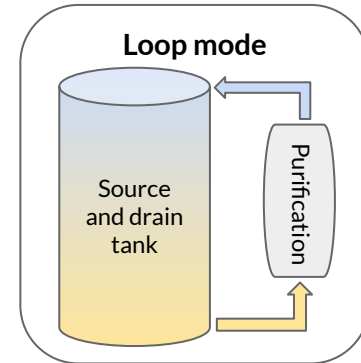
¹[R Acciarri et al. 2010 JINST 5 P05003]

²[R Acciarri et al. 2010 JINST 5 P06003]

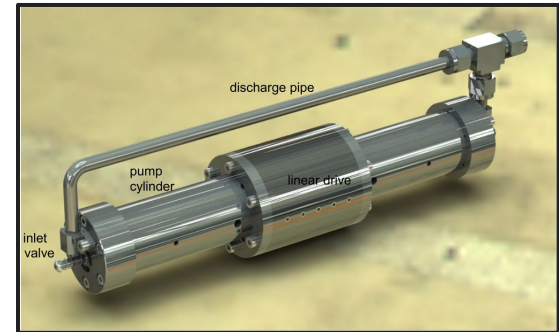
Application #2: Loop-mode purification of contaminated LAr

Triplet lifetime in SCARF reduced to $1.00 \pm 0.02 \mu\text{s}$ due to contamination with air

Upgrade of setup to accommodate loop-mode purification: Install **active LN₂ cooling** and use **submerged cryogenic liquid pump**



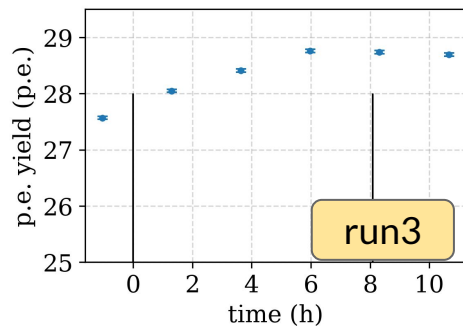
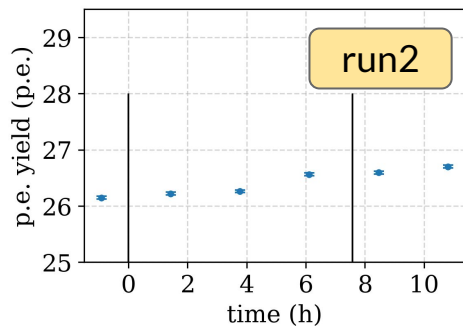
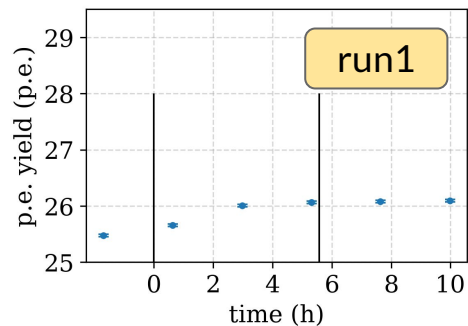
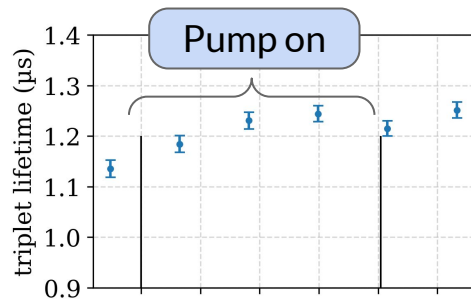
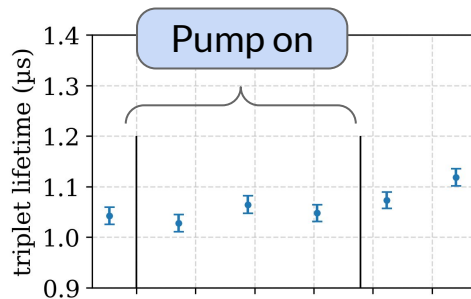
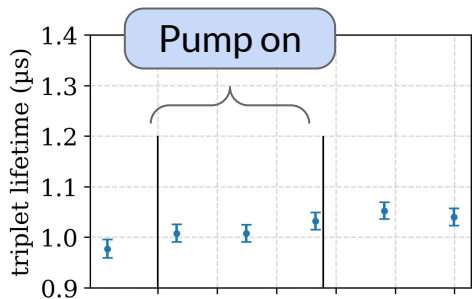
Purification cartridge wrapped in copper coil for active LN₂ cooling



Cryogenic submerged LAr pump

Single-day purification runs in loop mode

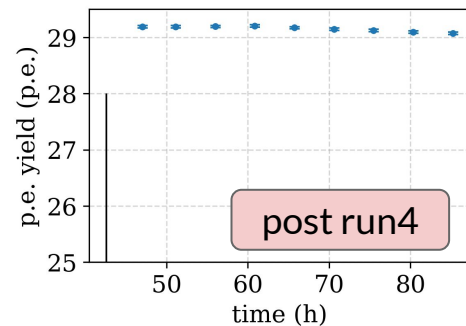
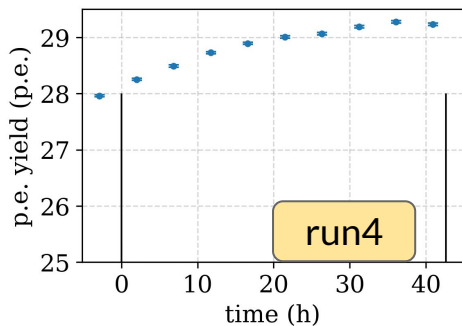
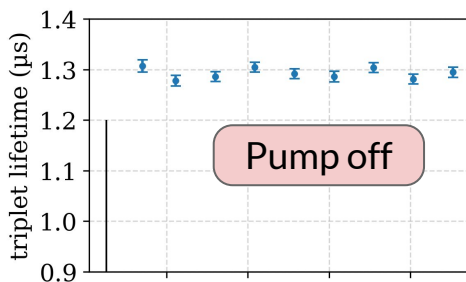
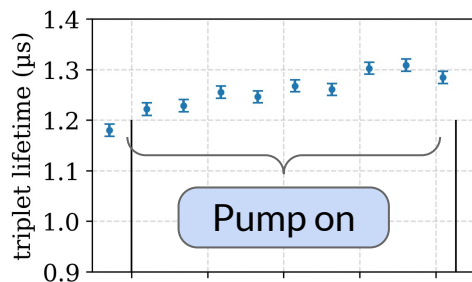
3 purification runs at different pumping speeds between 225 L/h to 450 L/h
Increase from $0.98 \pm 0.02 \mu\text{s}$ to $1.25 \pm 0.02 \mu\text{s}$ after ~ 9 volume exchanges



42 h purification run and aftermath

Long ~ 42 hour continuous purification run (10.4 volumes exchanged)

Increase back to ~ 1.3 μs ! Purification complete!



However, **photo-electron yield not completely recovered!**

29.21 \pm 0.02 p.e. after purification,
34.56 \pm 0.01 p.e. before contamination.

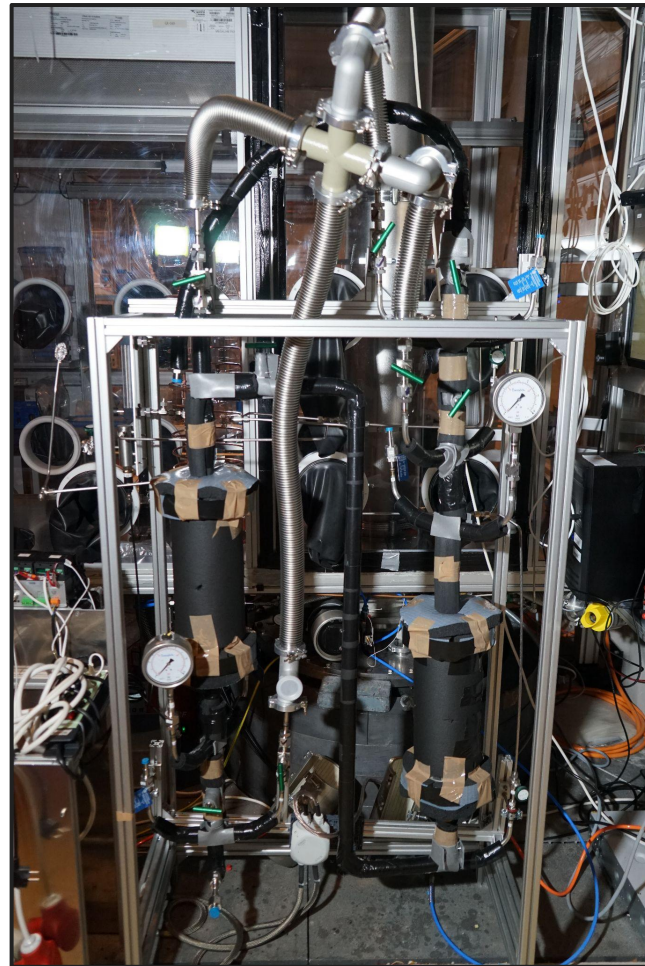
Origin unclear (as of yet)

¹[R Acciarri et al. 2010 JINST 5 P05003]

²[R Acciarri et al. 2010 JINST 5 P06003]

Conclusions

- High chemical purity is paramount for noble liquid detectors
→ on-site purification necessary
- We constructed a **LAr purification system** using dispersed **copper** and 4 A **molecular sieve**
- It purifies in **batch and loop mode** in liquid phase **to sub-ppm levels** (triplet lifetime $\sim 1.3 \mu\text{s}$)
- Outlook: Build model (improve understanding) of purification columns and provide vacuum insulation to reduce boil-off.



BACKUP

Regeneration procedure

Molecular sieve saturated with water:

Heat to ~ 250 °C and apply vacuum for a few hours.

Oxidized copper:

Heat to 200-250 °C and flush with hydrogen in low concentrations ($\leq 5\%$) in an inert carrier gas (e.g. nitrogen or argon) until some 100 cartridge volumes have been exchanged. Finally, apply vacuum.

Radon emanation from adsorbers

- O₂ adsorber (CU-0226 S 14 X 28): (0.43 ± 0.03) Bq/kg
- H₂O adsorber (MS 5A): (1.32 ± 0.04) Bq/kg

Loop mode purification details

Run #	Frequency	Volume flow	Duration	Total volume exchanged	# Cryostat volumes exchanged
1	3 Hz	450 L/h	5.6 h	2510 L	3.5
2	2 Hz	300 L/h	7.6 h	2280 L	3.2
3	1.5 Hz	225 L/h	8.1 h	1820 L	2.5
4a	1	150 L/h	28.5 h	4275 L	6.0
4b	1.5 Hz	225 L/h	14.1 h	3173 L	4.4
Sum	—	—	63.9	14058 L	19.6

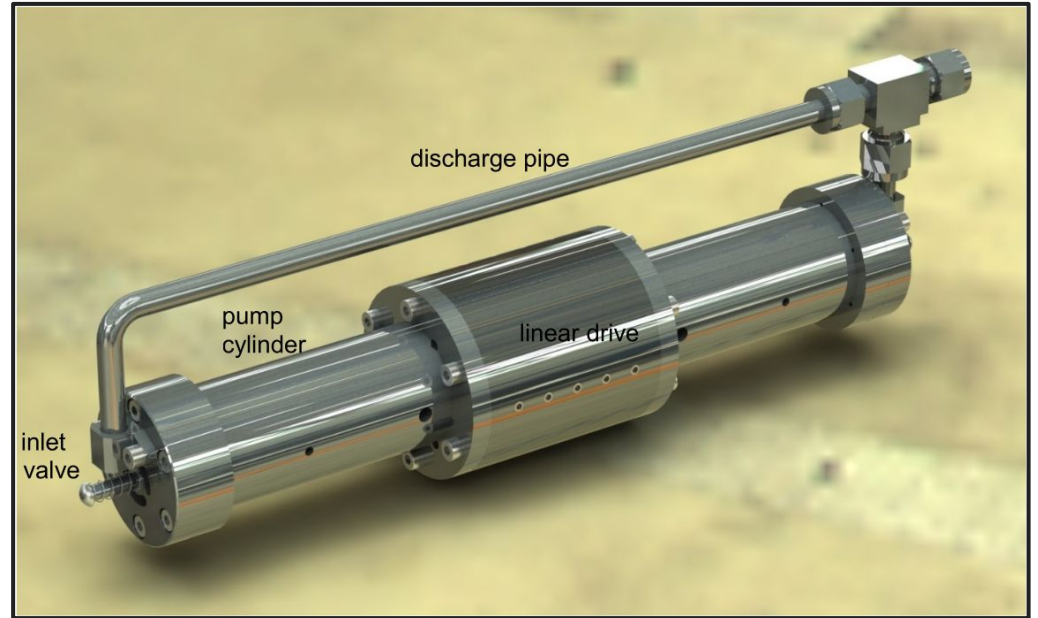
The LAr pump

Procured from the institute of
air handling and refrigeration
(IKL) Dresden

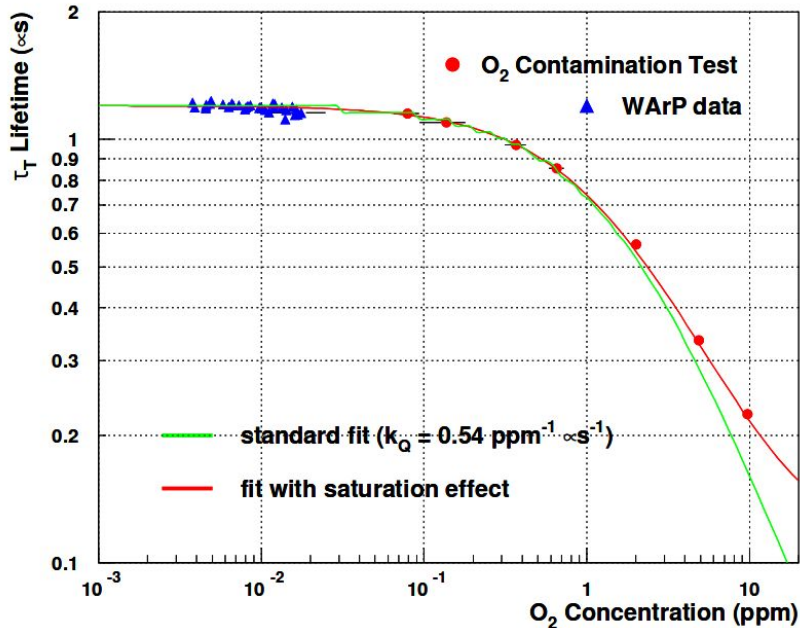
Linear drive piston pump.

Geometric flow rate of 150 L/h
@ 1 Hz operating frequency

Working frequency range: 0.5
Hz to 3.3 Hz, best performance
1 to 2 Hz



Contaminant removal in concentration (oxygen)



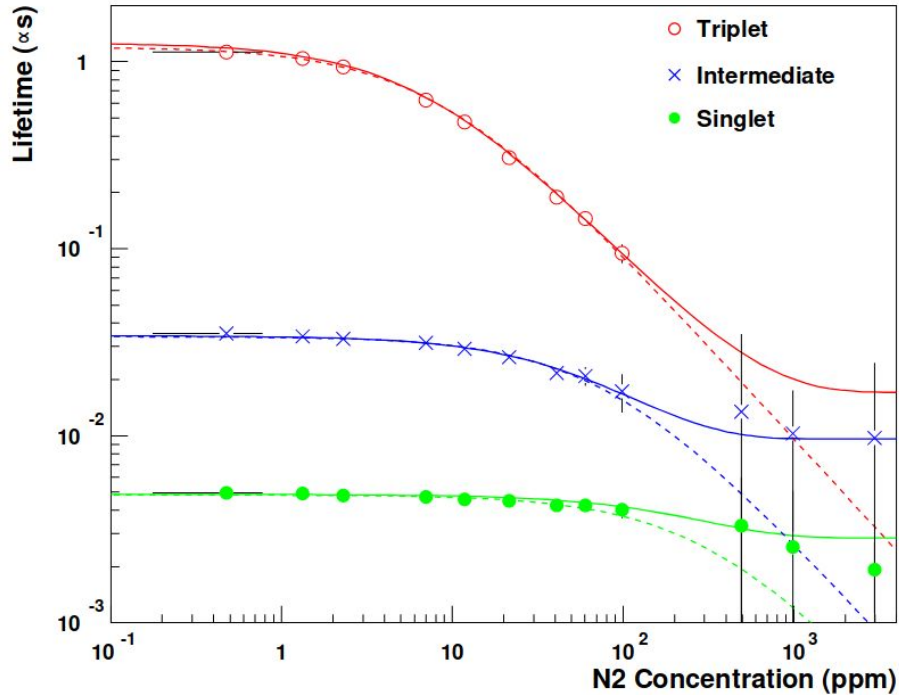
[R Acciarri et al 2010
JINST 5 P05003, fig. 6]

Assume that the contamination only stems from O_2 (not true, but provides a nice estimate)

Then we went from ~ 0.3 ppm O_2 equivalent before purification to < 0.01 ppm afterwards!

In loop mode!

Triplet lifetime and nitrogen concentration



[R Acciarri et al 2010
JINST 5 P06003, fig. 10]