



**TECHNISCHE
UNIVERSITÄT
DRESDEN**

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Cryogenic Refrigeration Efficiency Over a Large Range of Temperature

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ESSRI Madrid,
Sept. 26, 2024

History of (cryogenic) cooling



Ice harvest in winter / delivery / „cold box“



USA, NH₃ based
costs (1922): \$ 714
car (Ford Model T): \$ 450
average salary: \$ 2000 / yr

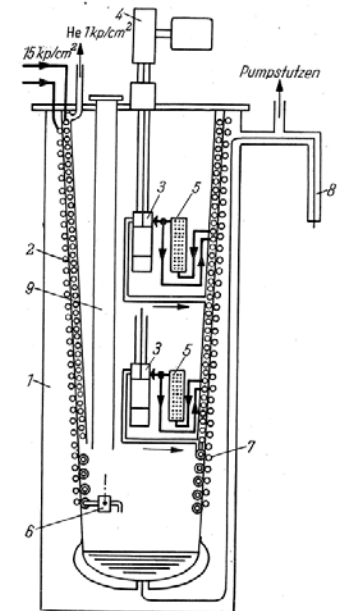


Household fridge becoming
widely available in Europe?
→ after WW II !

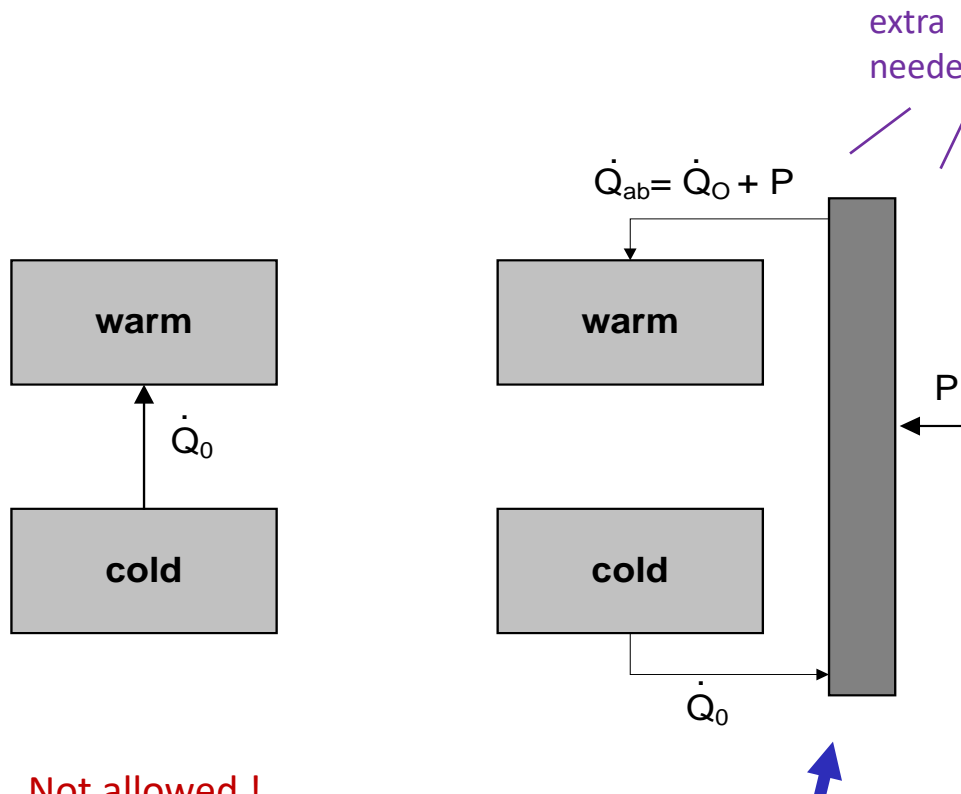
First Commercial Helium Liquefier



Prof. Sam Collins,
MIT/Boston → ADL comp.
1946



Theory of (Cryogenic) Cooling



Not allowed !
 OK for energy conservation;
 not OK for laws of thermodynamics

any kind of **Cooling Machine**

- working fluid/material
- „heat lift“ effect
- apparatus

extra $\Delta T \approx 3 \dots 5 \text{ K}$
 needed for heat transfer !

Demands:

- acceptance of entropy load
- transport (without further entropy production!)
- entropy transfer to ambient
 - a) continuous (circulation)
 - b) single shot (batch process)

Possible physical effect:

- gas compression / expansion
- fluid evaporation / condensation
- thermoelectric (Peltier)
- magnetocaloric (Gd, ...)
- thermoacoustic
- optic (Anti-Stokes)
- ...

Second law of thermodynamics (“Carnot”)

Refrigeration:

Minimum input power for
respective cooling power

$$P_{\min} = \dot{Q}_0 * \frac{T_U - T_0}{T_0}$$

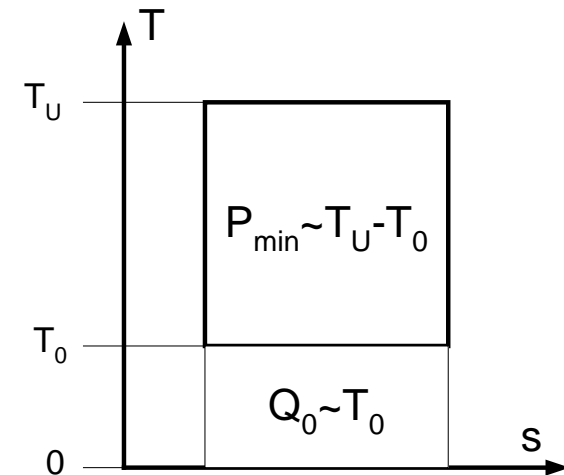
T_U Ambient temp.

T_0 Low temp.

T, s diagram:

P_{\min} vs. Q_0

graphically visible \Rightarrow



first headache: **Carnot Limit**

$$\text{COP}_{\text{carnot}} = \varepsilon_{\text{carnot}} =$$

$$Q_o / W = T_o / (T_u - T_o)$$

for $T_{\text{amb}} = 288 \text{ K}$:

$$T_o = 280 \text{ K} \Rightarrow \text{min } 0.03 \text{ W/W}$$

$$T_o = 77 \text{ K} \Rightarrow \text{min } 3 \text{ W/W}$$

$$T_o = 20 \text{ K} \Rightarrow \text{min } 13 \text{ W/W}$$

$$T_o = 4 \text{ K} \Rightarrow \text{min } 70 \text{ W/W}$$

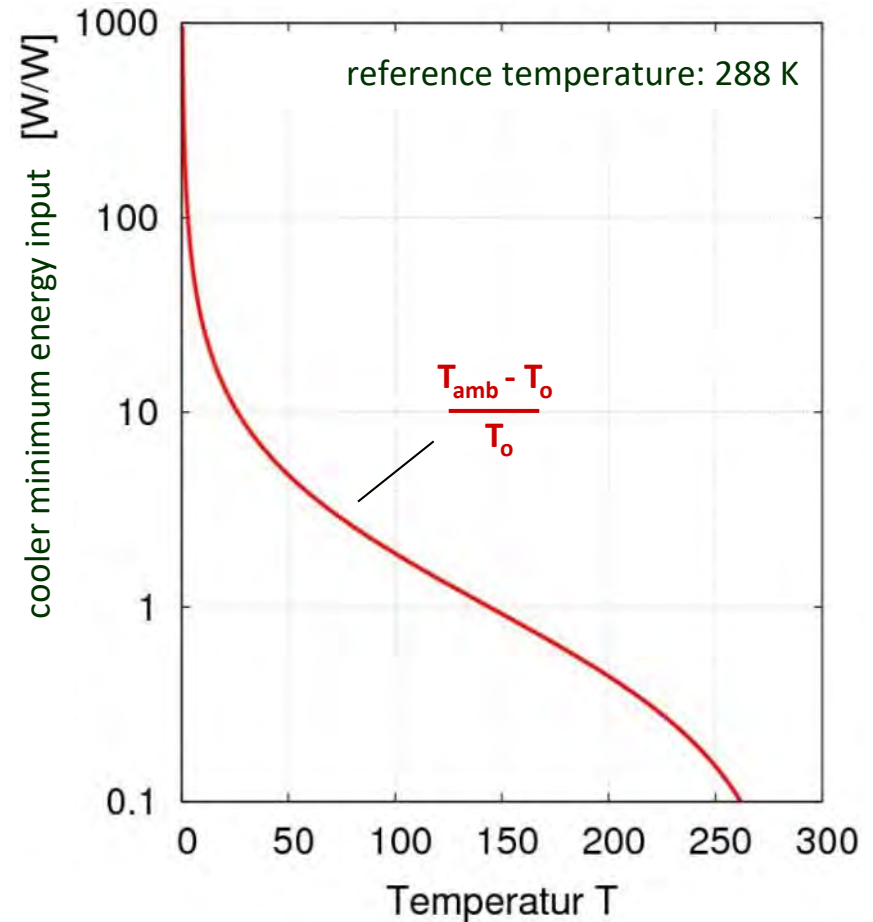
$$T_o = 2 \text{ K} \Rightarrow \text{min } 144 \text{ W/W}$$

$$T_o = 1 \text{ mK} \Rightarrow \text{min } 288 \text{ kW/W}$$

valid for ideal, reversible process
without any losses only !

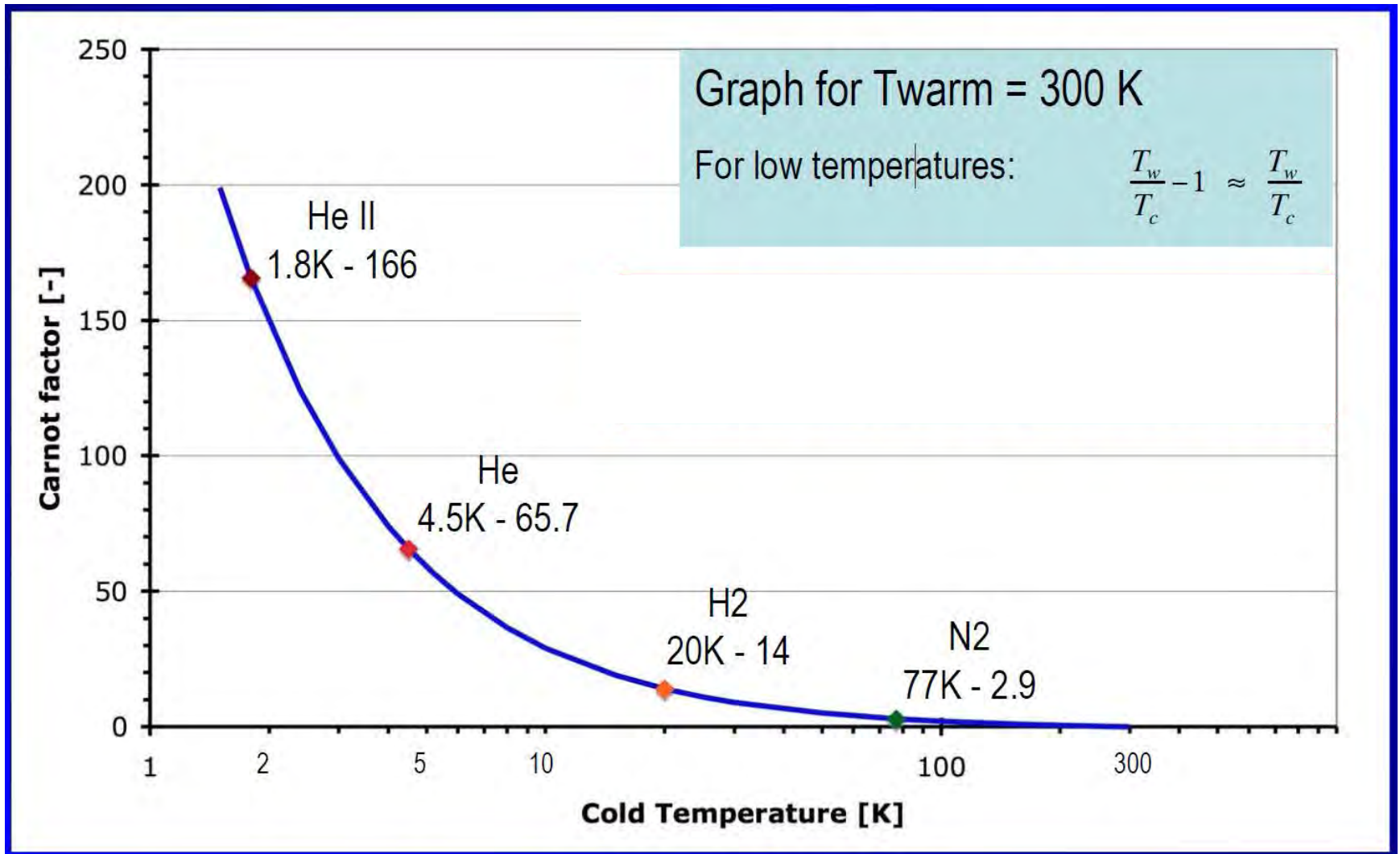
beware! Extra losses at cold and hot heat exchanger

($\Delta T \approx 3 \dots 5 \text{ K}$) ← unless e.g. bath cooling at low end temperature



first headache: **Carnot Limit**

Courtesy: Serge Claudet



Lesson learned from „Carnot“

- ⇒ The colder, the more energy expensive
- ⇒ Do not operate at temperatures lower than necessary
- ⇒ Minimize the heat load at very low temperatures

don't:

full heat load at
e.g. 4 K only

better:

thermal shields, intercepts
@ 80 K ⇐ by cheap LN₂
@ 20 K e.g.
minimum heat load at 4 K



trade-off: more complicated cooling plant / coldbox;
CAPEX vs. OPEX

second headache: Carnot Fraction

Carnot Fraction:

$$\text{Efficiency } \eta = \varepsilon_{\text{real}} / \varepsilon_{\text{Carnot}}$$

household refrigerator:

typ. 1 W/W $\Rightarrow \eta \approx 5\%$

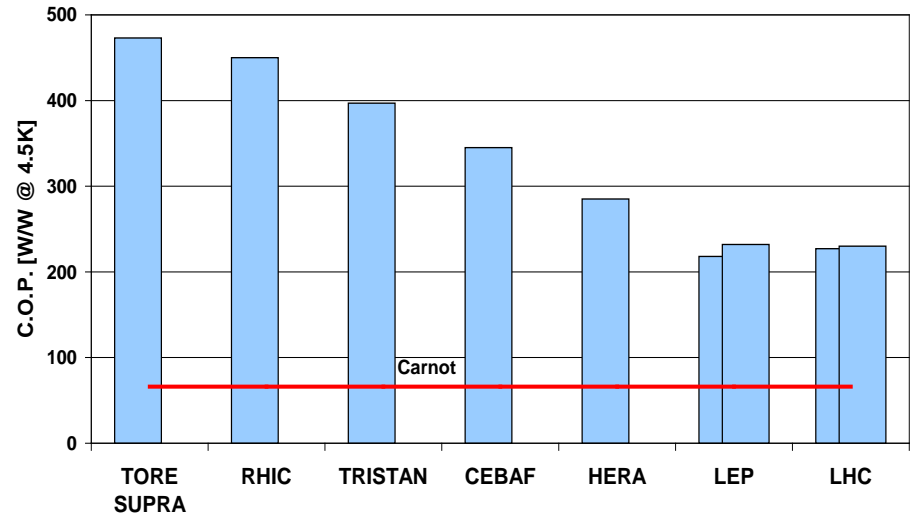
in cryogenics:

$\eta = 35\% \dots < 1\%$

e.g.: input power $P_{\text{el}} \approx 0.5 \text{ MW}$



cooling power @ 1.8 K: 200 W



COP – coefficient of performance

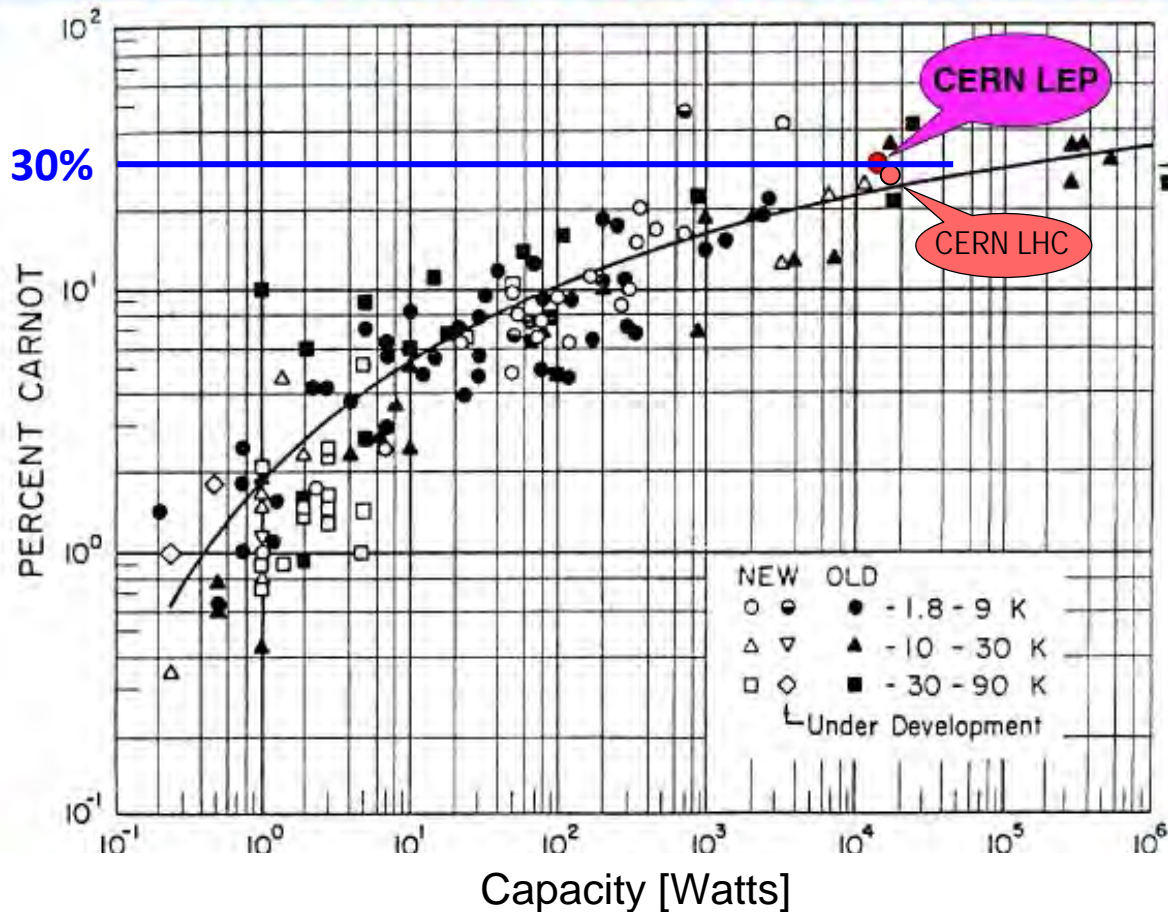
improvements achieved
for large cryogenic helium plants

Ph. Lebrun, CERN

second headache: Carnot Fraction

Courtesy:
Guy Gisteau;
Serge Claudet

LE DIAGRAMME DE STROBRIDGE



The efficiency w.r.t Carnot does not depend on the temperature, but rather on the size

Lesson learned from Strobridge:

⇒ A real cooling plant needs much more input power than a Carnot cycle (unavoidable)

⇒ The larger the cooling plant, the more efficient

⇒ better one large central cooling plant
then several distributed small local plants

⇒ Avoid „multiple“ safety factors

e.g. $\dot{Q}_o = 1.5 \times 1.5 \times 1.5$

safety factor
assigned by physicist

safety factor
assigned by
plant specification

safety factor
assigned by
plant manufacturer

all cryogenic
cooling plants
suffer a poor
part load efficiency

Why do we need such low temperatures after all?

a) condensation and liquefaction of gases

air separation; more easy transport and storage of N_2 , O_2 , H_2 , Ar, natural gas →

⇒ no interest in low temperatures, uneasy additional complication

Bonus: high purity gases



b) reduction of thermal noise and excitation

- undisturbed measurements in solid state physics, nuclear physics
- noise-reduced amplifiers
- all superconductive application

thermal excitation:

$$E = k \cdot T$$

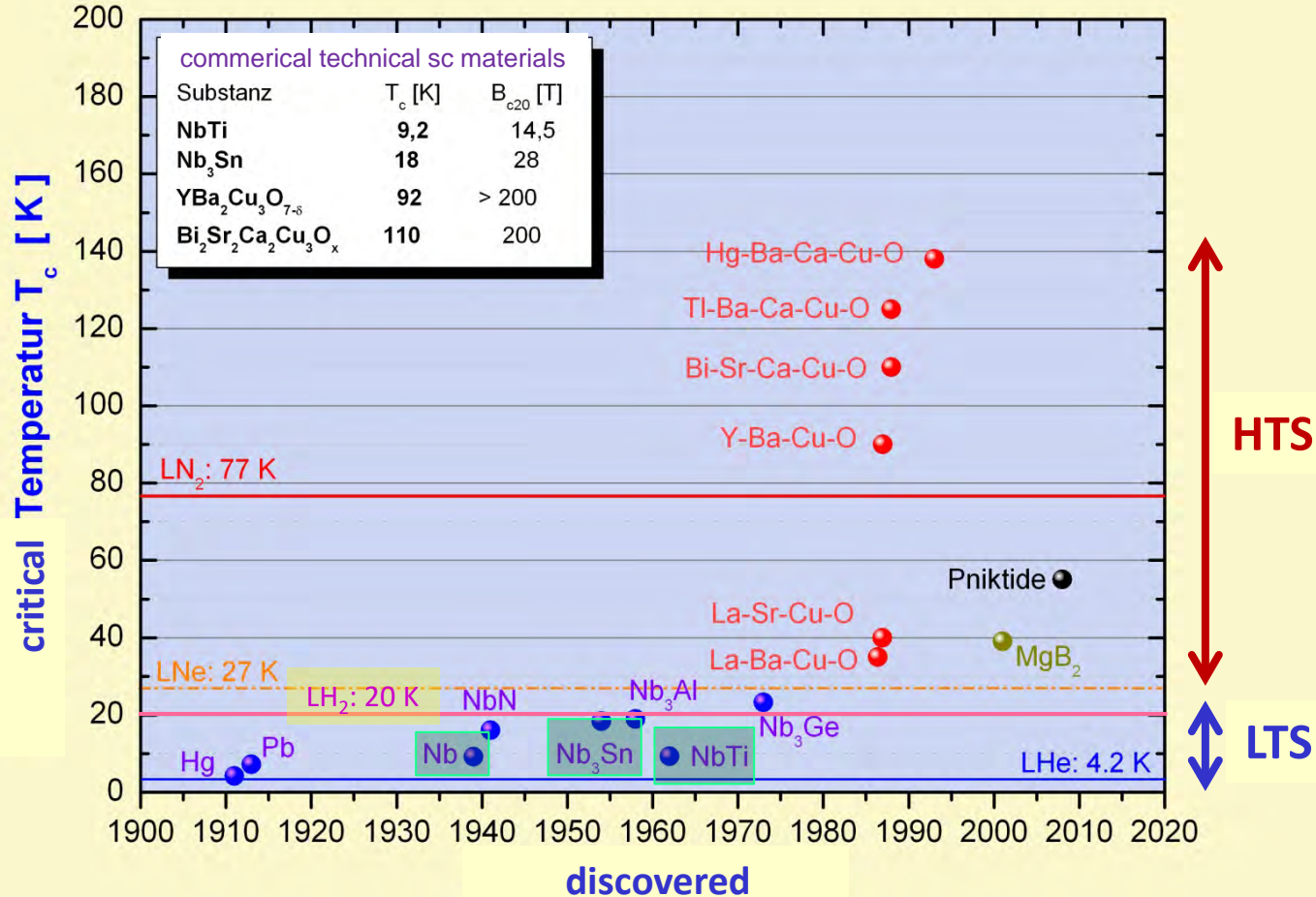
$$288 \text{ K: } k \cdot T = 25 \text{ meV}$$

$$4 \text{ K: } k \cdot T = 0.3 \text{ meV}$$

← close to binding energies in semi-conductors etc.

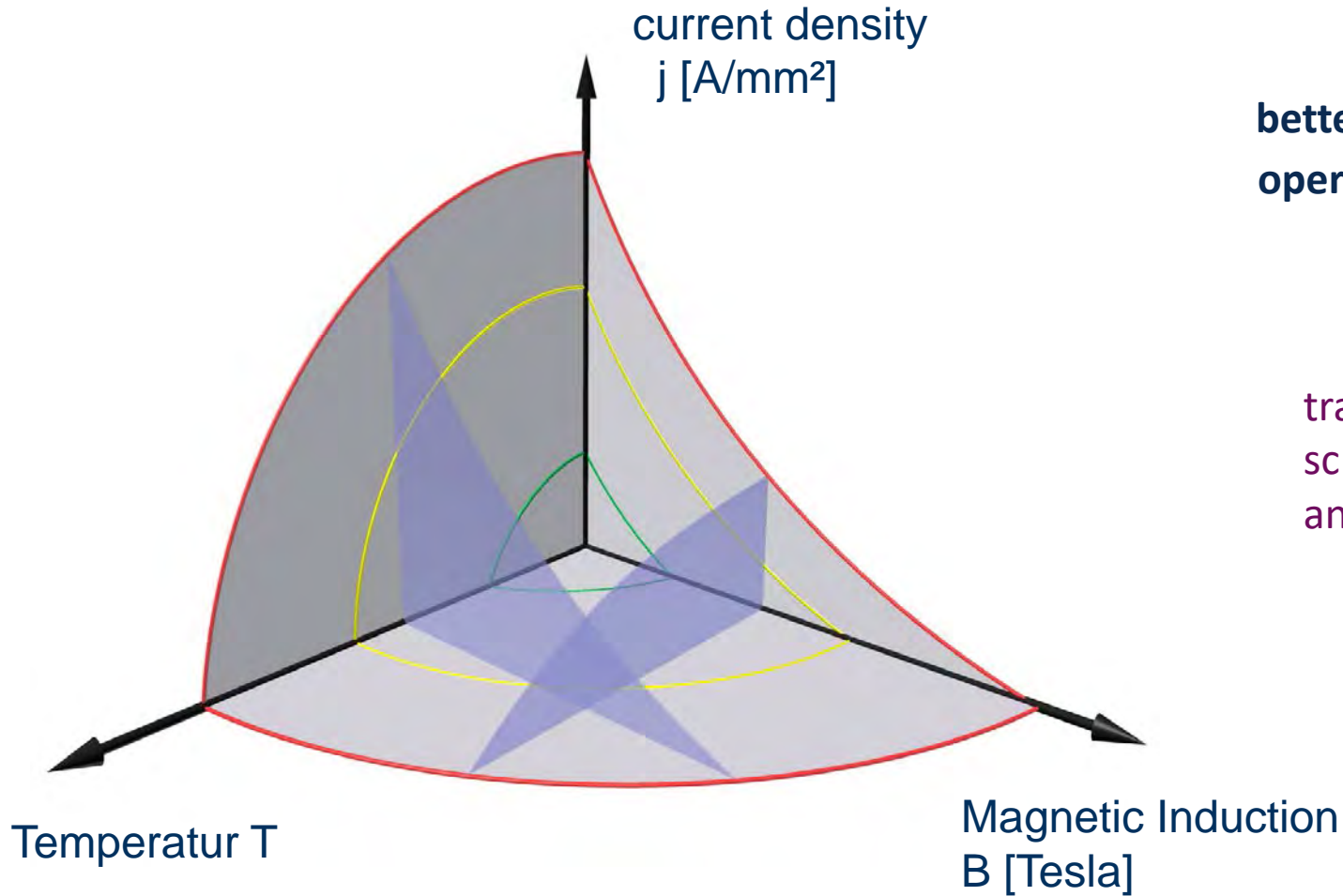
Superconducting materials

Courtesy:
Theo Schneider, KIT



nearly
exclusively
used

Technical Superconductors: Operational Limits



better j , B values when operated well below T_c



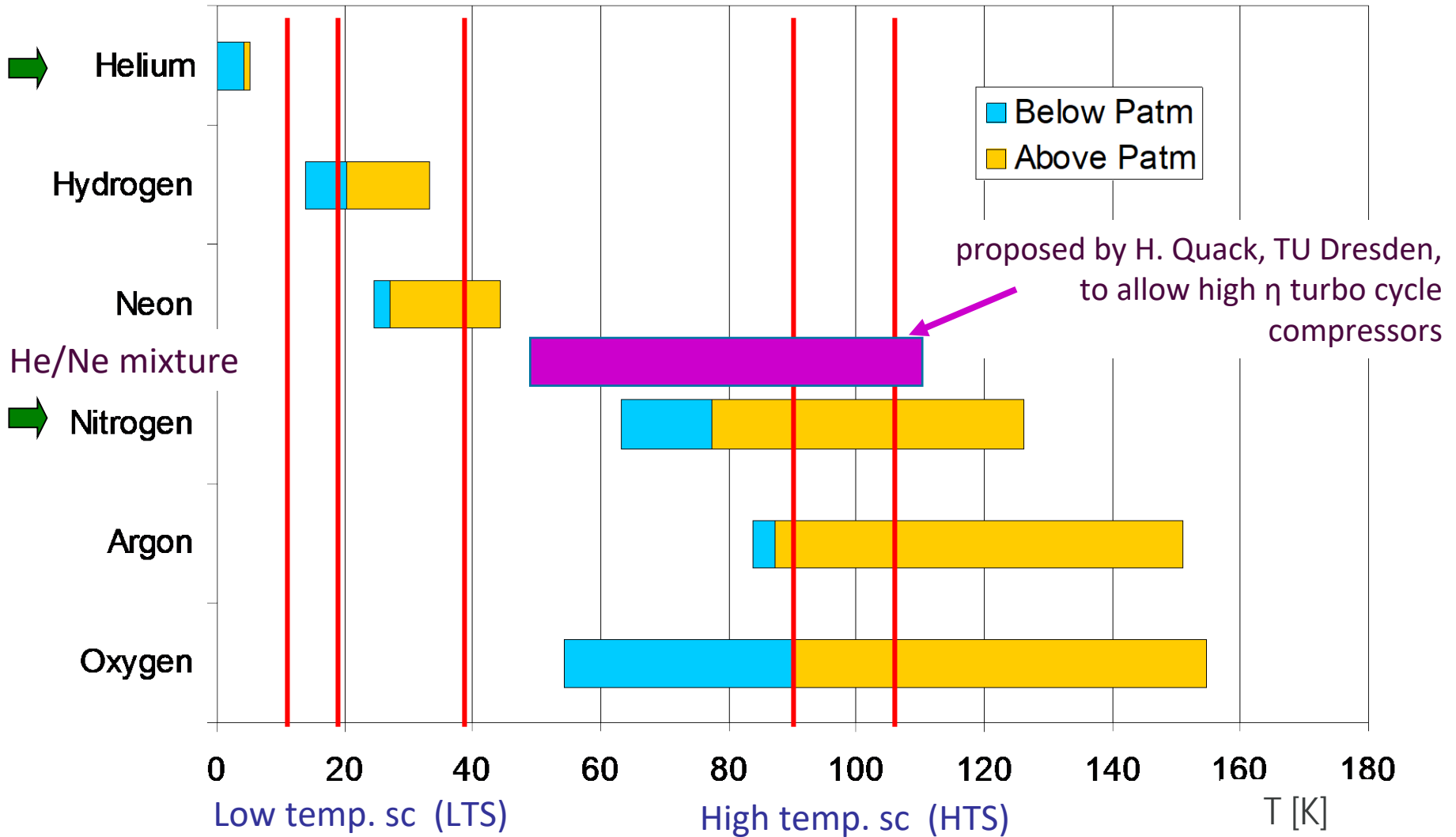
trade-off between sc performance and cooling effort

Cryogenic Fluids for Superconductor Cooling

Nb-Ti Nb₃Sn MgB₂

YBCO Bi-2223

Courtesy: Serge Claudet

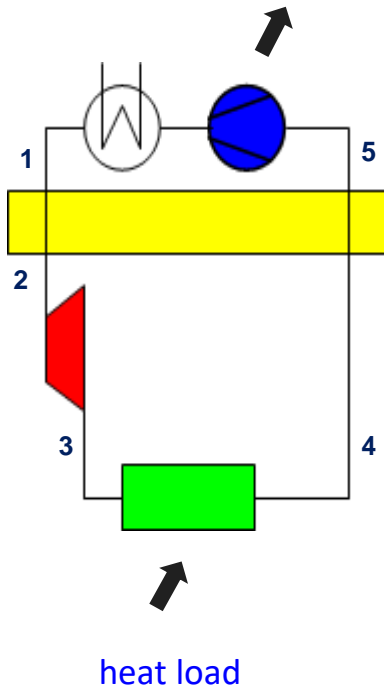


Cooling cycles with work extracting expansion

isentropic (work extracting) expansion: $\Delta S_{\text{ideal}} = 0$
(reversible)

\dot{m} small: volumetric expander (e.g. piston)
 \dot{m} large: turbines

Brayton Process



idealized:

isothermal compression
and heat release

isobaric
cool-down / warm-up

isentropic expansion

isothermal heat transfer

- + works always (ideal gas property)
- + much higher cooling effect
- mechanically demanding

real: isentropic efficiency η_s

$$\eta_s = \frac{h_2 - h_3}{h_2 - h_{3s}}$$

Cooling cycles with work extracting expansion

Expansion Turbines

axial + radial gas bearing; speed typ. 4500 s^{-1}



picture: Linde

recent optimization:

- geometry rotor / stator blades
- clearance losses
- material heat flow

isentropic efficiency

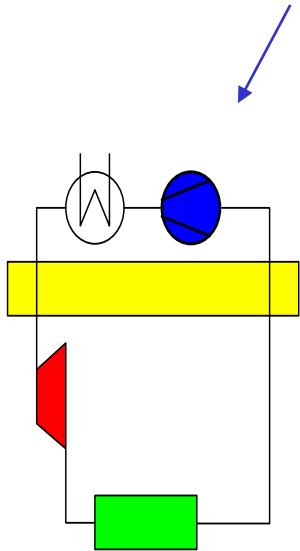
80th: $\eta_s \approx 65\%$

today: $\eta_s \approx 75 \dots 86\%$

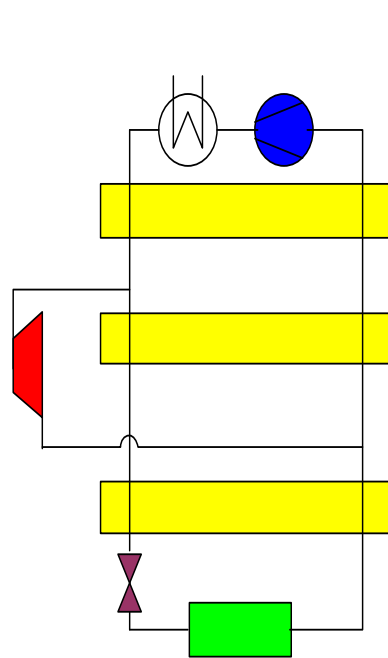
⇒ increase in cooling power by 1.5 ... 2

Basic Cryogenic Cycles

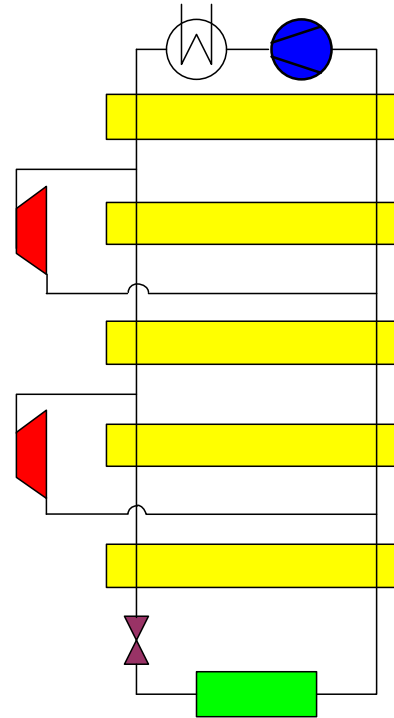
volumetric compressors
(oil lubricated screws); poor η
future: turbo machinery?



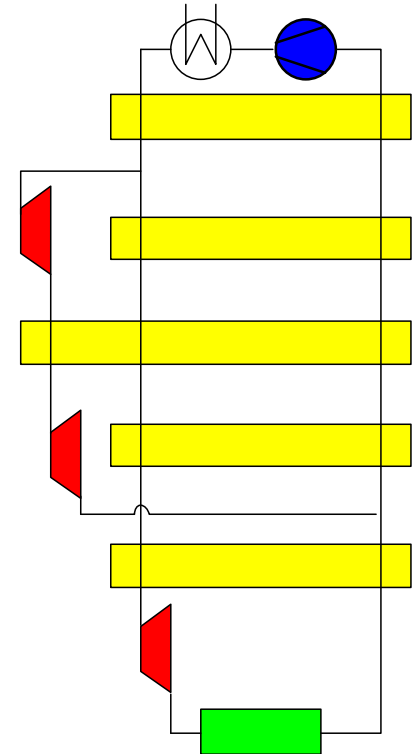
Brayton



Claude

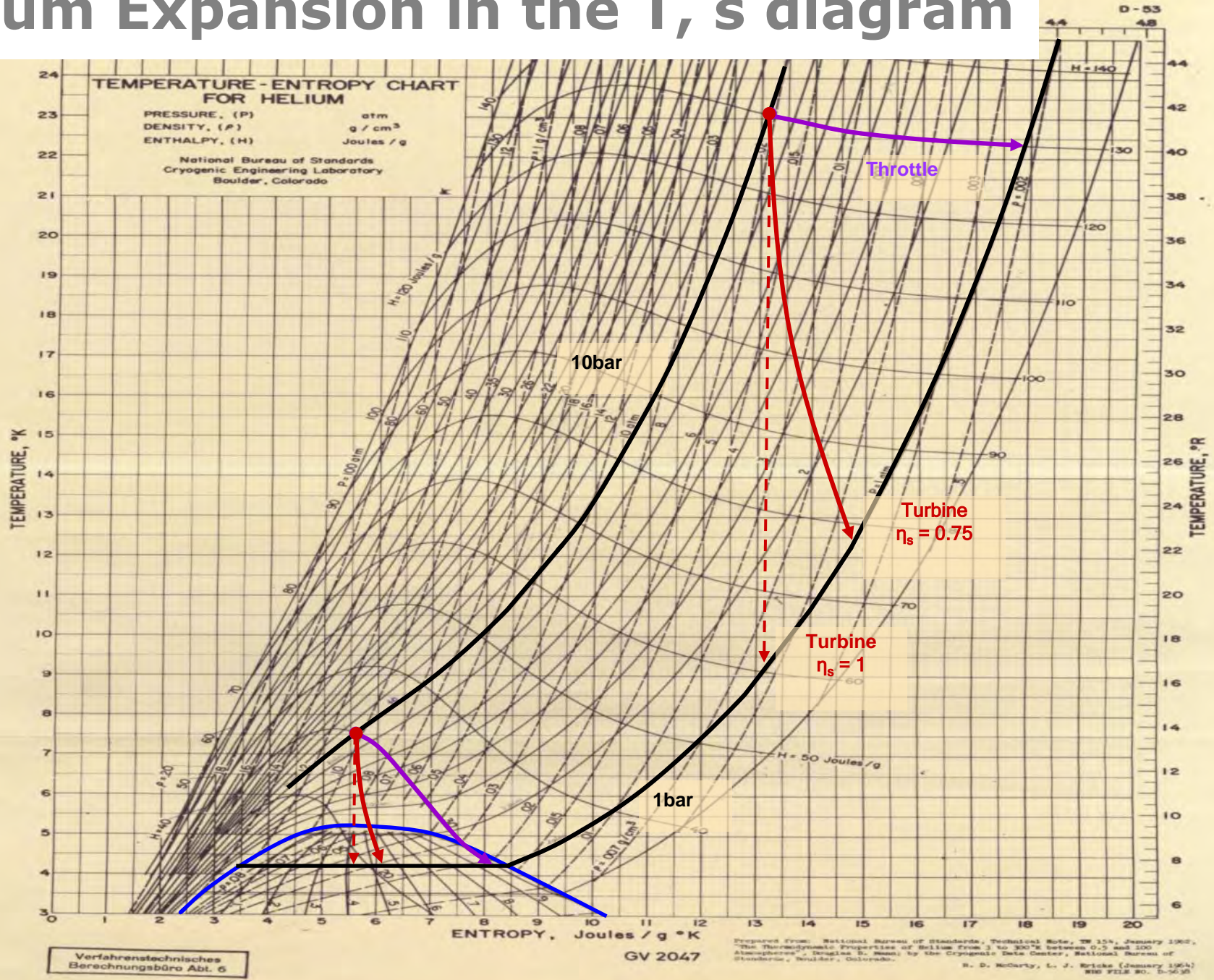


Expanders in parallel
(Collins)



Expanders in series
plus wet expander

Helium Expansion in the T, s diagram

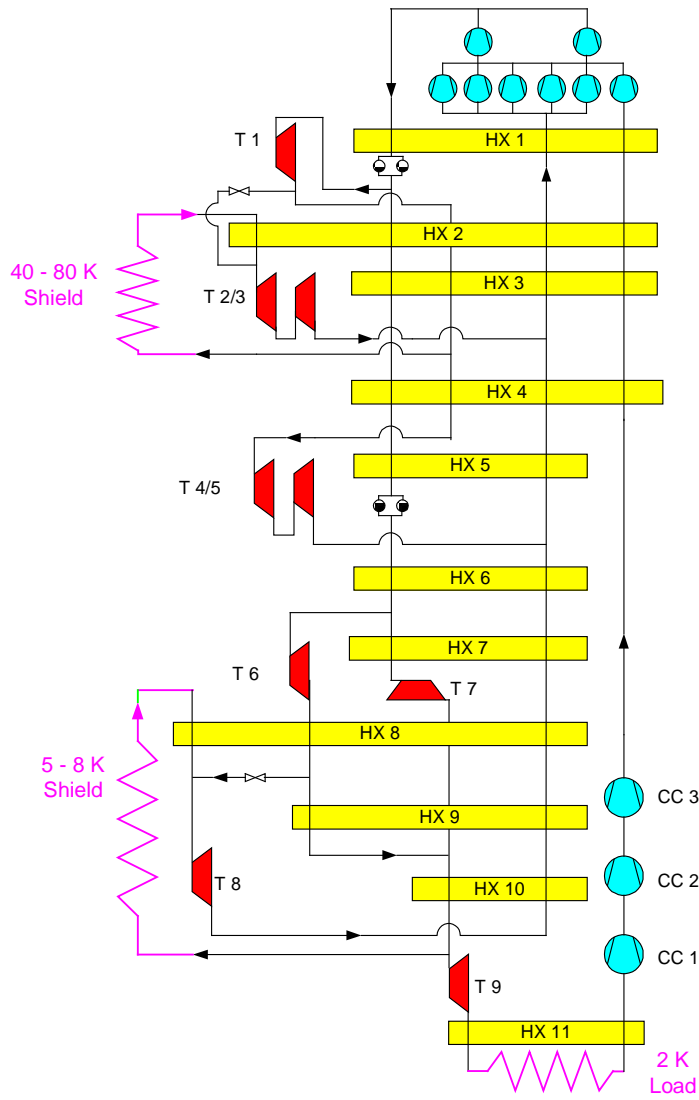


Verfahrenstechnisches
 Berechnungsbüro Abt. 6

GV 2047

Prepared from National Bureau of Standards, Technical Note, TN 154, January 1962, "The Thermodynamic Properties of Helium from 3 to 300°K between 0.5 and 100 Atmosphere", Douglas B. Mann, by the Cryogenic Data Center, National Bureau of Standards, Boulder, Colorado.
 H. D. Mcarty, L. J. Eriks (January 1964)
 NBS FILE NO. D-5630

Cooling cycles with work extracting expansion



“High-end” Helium Plant

Conceptual design for DESY, TESLA:

8 cycle compressors in two stages

9 expansion turbines

3 cold compressors

heat loads at three temperatur levels

to be operated 24/7

cool-down / warm up: days...weeks

shut-down once per year typically only

trade-off between

**CAPEX – Capital Expenditure
and plant efficiency**

Cryocooler as possible solution?

range, typically: „some Watt" @ 3 ... 100 K

- Stirling Cryocooler
- Gifford-McMahon Cooler
- Pulse Tube Cooler

well available

convenient, closed system

costs ~ 3000 ... 45000 €



e.g.: 18 W @ 20 K + 110 W @ 80 K; $P_{in} = 8 \text{ kW}$



Cryomech
PT450

5.0 W @ 4.2 K + 65 W @ 45 K

$P_{in} = 27 \text{ kW}$

Cryocooler as possible solution?

Cryocooler placed in a dewar's neck tube



alternative Helium Liquefaction:
Cryocooler + Dewar

Chao WANG, www.cryomech.com

HeRL15: > 15 l/day 1.5 W @ 4.2 K, $P_{el} = 9.2$ kW

↗
ca. 14 kWh / l_{LHe}

compare:

turbine liquefier
2 kWh / l_{LHe}

at least: can be switched
on/off on a few hours basis

ca. 100 000 300 000 € + yearly service

Thank you for
your attention!